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Making Measurement Science Work!

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TruTech Technical Training

Gauging your performance

Part III

The Next Generation





Energy Star on proper charge.

Refrigerant Charge

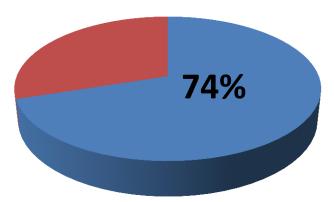
Essential to maintain capacity to 41% systems and **d**vercharged - System with more than ±3° deviction in s sp c would not



California PUC analysis of 13,000 residential and commercial units

- Most off by ½ to 5 pounds of refrigerant
- A/C units off by more than 8 ounces will potentially fail within 5 years
- In cap tube or short orifice systems even one or two ounces can have a serious impact on performance





74% of systems are improperly charged

Causes

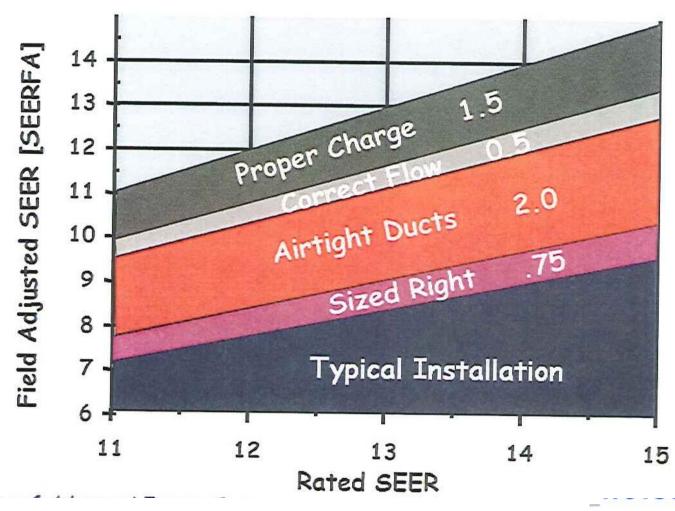
- •Improperly calibrated measurement equipment
- •Human errors during commissioning

SOURCE: The California refrigerant and airflow verification program



ENERGY STAR INDOOR AIR PACKAGE HVAC BEST PRACTICE INSTALLATION





Commissioning the system

Getting the Charge Correct

- Set airflow
- ID metering device
- Charge by superheat or subcooling
- Check the split across the evaporator
- Document the operation





Matched components:

-Systems must be listed in the ARI directory

Increased importance of charging:

- -Proper charge is imperative to get guaranteed energy efficiency, capacity, and system reliability.
- –A few ounces of refrigerant changes everything!!!!!

Critical airflows:

- -Airflow directly effects efficiency, capacity, and creature comfort.
- Proper airflow across the evaporator is critical to achieve efficiency ratings.

Set Airflow (nominal)

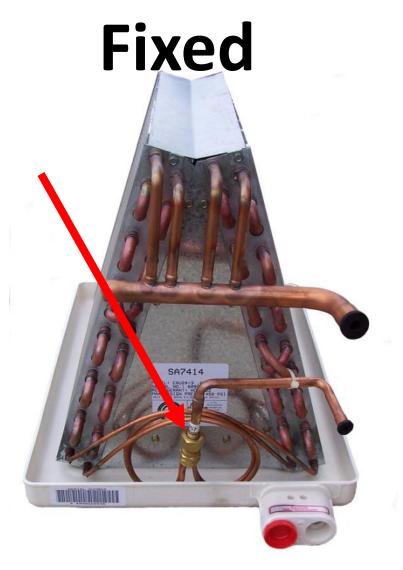


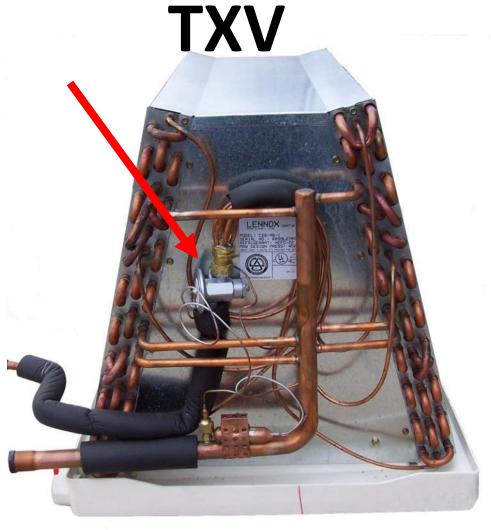
	BTUh	Airflow
•	12,000	400 CFM
•	18,000	600 CFM
•	24,000	800 CFM
•	30,000	1000 CFM
•	36,000	1200 CFM
•	42,000	1400 CFM
•	48,000	1600 CFM
•	60,000	2000 CFM





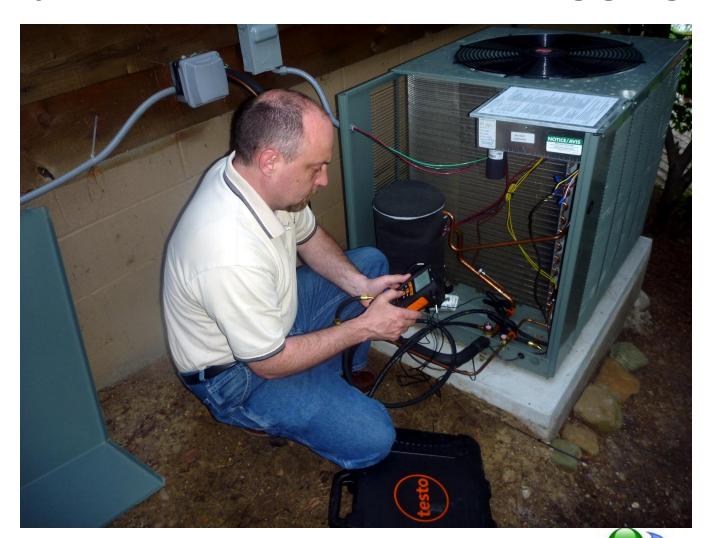
ID the metering device







The Digital Dilemma Do you need to switch from analog gauges?



I lech Tools

Without need there is nothing but fluff

- Do technicians really need digital gauges?
- What's wrong with the way I have been charging?
- Are there really any benefits aside from a "digital" display?
- How many systems suffer from incorrect charge?
- Are they expensive to buy and maintain?
- Are they reliable?
- Are they easy to use?





Are there really problems with Analog Instruments?

Just the facts, mam. Just the facts.





Old School Tools

Tools of the Trade

- •Gauges for each refrigerant
- •Temperature pressure chart
- •Thermometer
- Calculator
- •Pen
- Paper





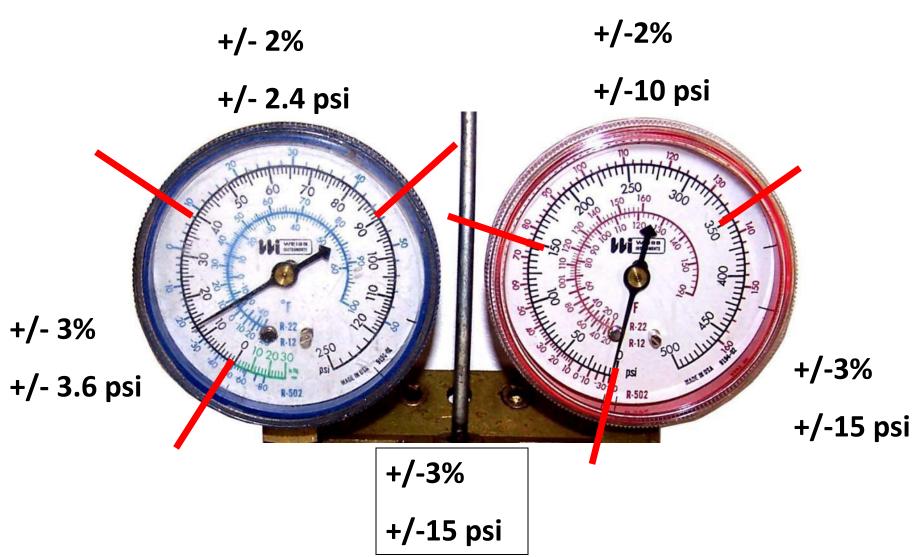
Current refrigeration gauges

- Are using the same technology for the last century and a half!
 - Albeit, today more precisely manufactured
- With much care can produce readings that are OK
- Were in specification when they left the factory
 - Only to +/-3%, +/-2%, +/-3 %
 - But is close enough, good enough?





Standard 3-2-3 Gauges





So what about 1% accuracy???



+/-3.5 psi

+/-8.0 psi



Vacuum-Inches of Mercury Italic Figures



TEMPERATURE PRESSURE CHART - at sea level

Pressure-Pounds Per Square Inch Gauge **Bold** Figures

TEAMPERATURE DEEDICERANT (CROPI AN CORE)							TELLEGO LTUDE DESCRIPTION AND AND AND AND AND AND AND AND AND AN										
	PERATURE REFRIGERANT (SPORLAN CODE)				TEMPERATURE REFRIGERANT (SPORLAN CODE)			TEMPERATURE REFRIGERANT (SPORLAN CODE)									
۰F	°C	R-22(V)		R-407C(N)		°F	°C	R-22(V)	R-410A(Z)	R-407C(N)	R-134a(J)	۰F	°C	R-22(V)		R-407C(N)	R-134a(J)
-60	-51.1	11.9	0.9	16.0	21.6	12	-11.1	34.8	65.4	29.0	13.2	42	5.6	71.5	123.6	64.6	37.0
-55	-48.3	9.2	1.8	13.7	20.2	13	-10.6	35.8	67.0	29.9	13.8	43	6.1	73.0	125.9	66.1	38.0
-50	-45.6	6.1	4.3	11.1	18.6	14	-10.0	36.8	68.6	30.9	14.4	44	6.7	74.5	128.3	67.6	39.0
-45	-42.8	2.7	7.0	8.1	16.7	15	-9.4	37.8	70.2	31.8	15.1	45	7.2	76.1	130.7	69.1	40.0
-40	-40.0	0.6	10.1	4.8	14.7	16	-8.9	38.8	71.9	32.8	15.7	46	7.8	77.6	133.2	70.6	14.1
-35	-37.2	2.6	13.5	1.1	12.3	17	-8.3	39.9	73.5	33.8	16.4	47	8.3	79.2	135.6	72.2	42.2
-30	-34.4	4.9	17.2	1.5	9.7	18	-7.8	40.9	75.2	34.8	17.1	48	8.9	80.8	138.2	73.8	43.2
-25	-31.7	7.5	21.4	3.7	6.8	19	-7.2	42.0	77.0	35.9	17.7	49	9.4	82.4	140.7	75.4	44.3
-20	-28.9	10.2	25.9	6.2	3.6	20	-6.7	43.1	78.7	36.9	18.4	50	10.0	84.1	143.3	77.1	45.4
-18	-27.8	11.4	27.8	7.2	2.2	21	-6.1	44.2	80.5	38.0	19.2	55	12.8	92.6	156.6	106.0	51.2
-16	-26.7	12.6	29.7	8.4	0.7	22	-5.6	45.3	82.3	39.1	19.9	60	15.6	101.6	170.7	116.2	57.4
-14	-25.6	13.9	31.8	9.5	0.4	23	-5.0	46.5	84.1	40.2	20.6	65	18.3	111.3	185.7	127.0	64.0
-12	-24.4	15.2	33.9	10.7	1.2	24	-4.4	47.6	85.9	41.3	21.4	70	21.1	121.5	201.5	138.5	71.1
-10	-23.3	16.5	36.1	11.9	2.0	25	-3.9	48.8	87.8	42.4	22.1	75	23.9	132.2	218.2	150.6	78.6
-8	-22.2	17.9	38.4	13.2	2.8	26	-3.3	50.0	89.7	43.6	22.9	80	26.7	143.7	235.9	163.5	86.7
-6	-21.1	19.4	40.7	14.6	3.7	27	-2.8	51.2	91.6	44.7	23.7	85	29.4	155.7	254.6	177.0	95.2
-4	-20.0	20.9	43.1	15.9	4.6	28	-2.2	52.4	93.5	45.9	24.5	90	32.2	168.4	274.3	191.3	104.3
-2	-18.9	22.4	45.6	17.4	5.5	29	-1.7	53.7	95.5	47.1	25.3	95	35.0	181.9	295.0	206.4	113.9
0	-17.8	24.0	48.2	18.9	6.5	30	-1.1	54.9	97.5	48.4	26.1	100	37.8	196.0	316.9	222.3	124.1
1	-17.2	24.8	49.5	19.6	7.0	31	-0.6	56.2	99.5	49.6	26.9	105	40.6	210.8	339.9	239.0	134.9
2	-16.7	25.7	50.9	20.4	7.5	32	0	57.5	101.6	50.9	27.8	110	43.3	226.4	364.1	256.5	146.3
3	-16.1	26.5	52.2	21.2	8.0	33	0.6	58.8	103.6	52.1	28.6	115	46.1	242.8	389.6	274.9	158.4
4	-15.6	27.4	53.6	22.0	8.6	34	1.1	60.2	105.7	53.4	29.5	120	48.9	260.0	416.4	294.2	171.1
5	-15.0	28.3	55.0	22.8	9.1	35	1.7	61.5	107.9	54.8	30.4	125	51.7	278.1	444.5	314.5	184.5
6	-14.4	29.1	56.4	23.7	9.7	36	2.2	62.9	110.0	56.1	31.3	130	54.4	297.0	474.0	335.7	198.7
7	-13.9	30.0	57.9	24.5	10.2	37	2.8	64.3	112.2	57.5	32.2	135	57.2	316.7	505.0	357.8	213.5
8	-13.3	31.0	59.3	25.4	10.8	38	3.3	65.7	114.4	58.9	33.1	140	60.0	337.4	537.6	380.9	229.2
9	-12.8	31.9	60.8	26.2	11.4	39	3.9	67.1	116.7	60.3	34.1	145	62.8	359.1	571.7	405.1	245.6
10	-12.2	32.8	62.3	27.1	12.0	40	4.4	68.6	118.9	61.7	35.0	150	65.6	381.7	607.6	430.3	262.8
11	-11.7	33.8	63.9	28.0	12.6	41	5.0	70.0	121.2	63.1	36.0	155	68.3	405.4	645.2	456.6	281.0

To determine subcooling for refrigerant R-407C use BUBBLE POINT values (Temperatures above 50°F — Gray Background); to determine superheat R-407C, use DEW POINT values (Temperatures 50°F and below).



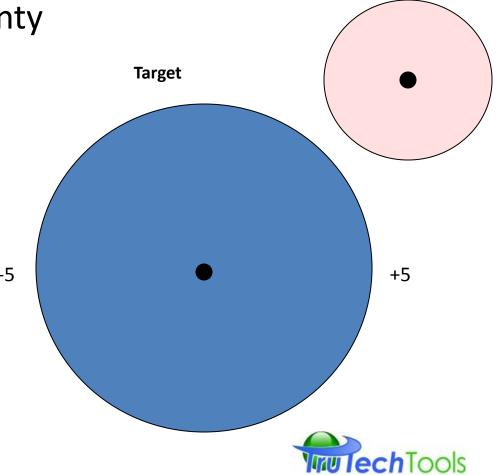


Measurement Accuracy

Is close enough good enough?

Every method has the a target and measurement uncertainty

- Superheat
- Subcooling
- Wet-bulb
- Dry-bulb
- Line temperatures



Measurement

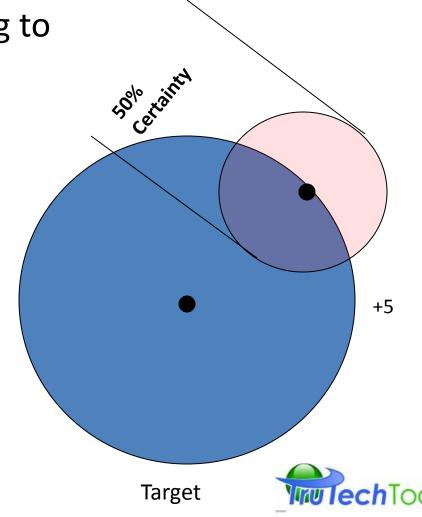
Uncertainty

Measurement Accuracy

Is close enough good enough?

Charging to the target for most technicians means getting to the edge.

Within 5° for superheat for example can still have an uncertainty of 50%



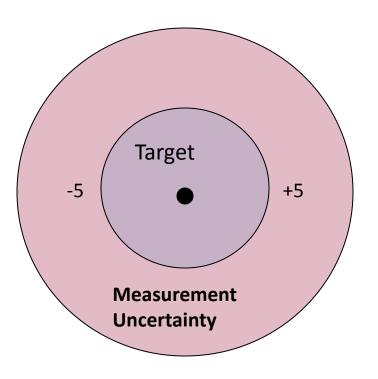
Measurement Accuracy

Is close enough good enough?

Analog technology and related inherent error make the uncertainty overshadow the target.

Causes:

- Substandard
- Out of calibration
- Lack of training
- Incorrect measuring techniques





Measurement Uncertainty

- K-type +/- 4°F
- Gauge (psi)
 +/- 2.4 to 3.5 low side
 +/- 8 to 10 high side

Both easily loose calibration and accuracy, voltage effect on thermocouples



- Thermistor +/- 1.8°F
- Transducer +/- 2.5 psi
 - Temperature compensated
 - Altitude compensated

Excellent Long term stability and accuracy







SOURCE: The International Journal of Sensing for Industry Volume 21, No. 3 2001.

	Thermocouple	RTD (Pt100)	Thermistor	
Operating Range	-200 °C to 2000 °C	-250 to 850 °C	-100 to 300 °C	
Accuracy	Low 1 °C common	Very High 0.03 °C common	High 0.1°C common	
Linearity*	Medium	High	Low	
Thermal Response**	Fast	Slow	Medium	
Cost	Low	High	Low to moderate	
Noise Problems	High	Medium	Low	
Long term stability	Low	High	Medium	
Cost of measuring instrument	Medium	High	Low	

^{*} Linearity is not an issue if using modern digital measuring instruments, as look-up tables stored in memory provide compensation.



^{**} Thermal response is considered for the measuring element only, not its enclosure.

Condensing Temps Analog

1-2% accuracy (+/- 8-10 PSI)

- (°F) R410a R-22
- <u>105 339.6 210.8</u>
- 106 344.4 213.8
- <u>107</u> <u>349.3</u> <u>216.9</u>
- 108 354.2 220.0
- <u>109 359.1 223.2</u>
- 110 364.1 226.4
- <u>111 369.1 229.6</u>
- 112 374.2 232.8
- <u>113 379.4</u> <u>236.1</u>

- R22@ 220 psig (+/- 10 PSI @2%)
 - Low 105, high 111+/- 3°F saturation
- R410a @ 359 psig (+/-8 PSI @1%)
 - Low 107, high 111+/- 2° saturation
- Temp +/- 4°F

10°F max Uncertainty R22 8°F max Uncertainty 410a



Condensing Temps Digital 0.5% accuracy (+/- 2.5 PSI)

- (°F) R410a R-22
- <u>105 339.6 210.8</u>
- 106 344.4 213.8
- 107 349.3 216.9
- <u>108 354.2 220.0</u>
- <u>109 359.1 223.2</u>
- 110 364.1 226.4
- <u>111 369.1 229.6</u>
- 112 374.2 232.8
- <u>113 379.4</u> <u>236.1</u>

- R22@ 220 psig (+/- 2.5 PSI @0.5%)
 - Low 107.5, high 109
 - +/- <1°F saturation temp (calc)
- R410a @ 359 (+/- 2.5 PSI @0.5%)
 - Low 108.5, high 110+/- <0.5°F saturation temp (calc)
- Temp +/- 1.8°F
- 2.3-2.8° max Uncertainty for R22 or 410a



Charging Accuracy

Is close enough good enough?

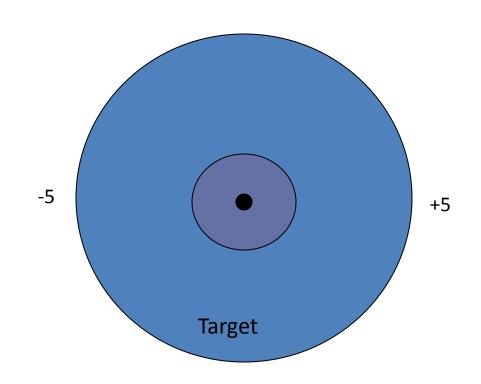
With Digital Gauges

Smaller uncertainty

Higher accuracy

Human factor is reduced or eliminated

Probability of correct charge significantly increased.





Allowed range as a function of superheat and subcooling measured uncertainty

Uncertainty in measured Superheat	Adjusted Allowed	Uncertainty in	Adjusted Allowed
	Superheat	measured	Subcooling
	(target – measured)	Subcooling	(target – measured)
± 0.0 ° F ± 1.0 ° F ± 2.0 ° F ± 3.0 ° F ± 4.0 ° F ± 5.0 ° F	± 5.0 ° F ± 4.1 ° F ± 3.2 ° F ± 2.3 ° F ± 1.4 ° F ± 0.5 ° F	± 0.0 °F ± 1.0 ° F ± 2.0 ° F ± 3.0 ° F	± 3.0 °F ± 2.1 °F ± 1.2 °F ± 0.1 °F

HVAC Energy Efficiency Maintenance Study

Issued: December 29, 2010

By the Davis Energy Group and the WCEC (Western Cooling Efficiency Center)



Digital does it better!

- Allows trending & more complex functions
- Higher accuracy reduces callbacks
- Calculates without human error
- Stays in calibration
- High reliability
- Excellent repeatability





Thick Film Pressure Transducers

- High chemical compatibility
- Resistant to corrosion
- High linearity and low hysteresis
- Wide temperature range
- High long term stability
- 0.5% full scale accuracy
- •+/- 2.5 psi high and low side
- Temperature compensated







Charging the system

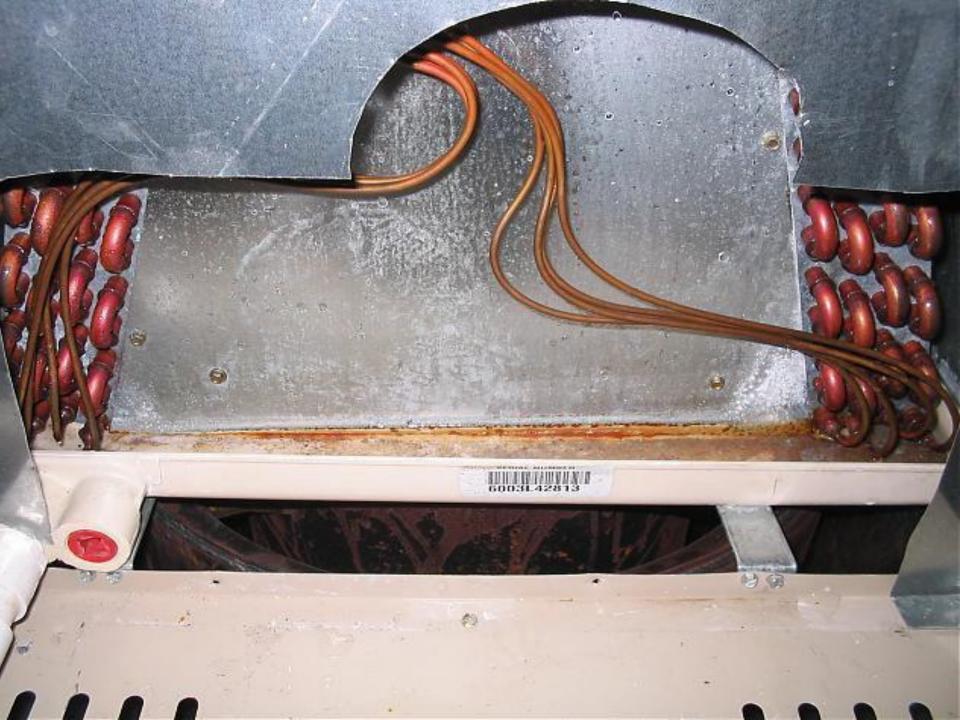
- The proper mass of refrigerant that allows the system to operate at its optional state for reliability, capacity and efficiency
 - Verified by superheat and subcooling
 - Weighing in the charge does not guarantee proper operation

Remember

Think clean

Look for the obvious













Notes on Charge

- Systems come with enough refrigerant for a matched coil and typically 15' of line set
- Length and lift can impact charging requirements
- Consult manufacturer's instructions for line sets over 50'





Weigh in is Best

sometimes

- Correct Charge must be known!
- Can be done all year
- Airflow must be set prior to evaluating charge
- Must be evaluated under proper conditions
 - Must have proper indoor load
- Check both the superheat and the subcooling!



Does not guarantee proper operation!



The Fixed Orifice System



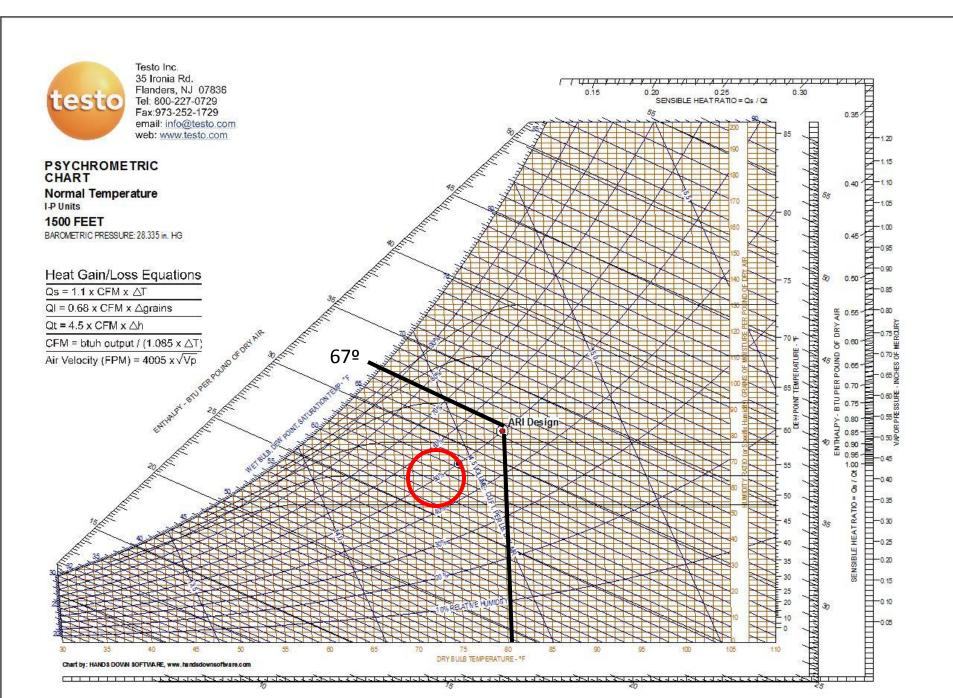


AHRI Design Conditions

- •80° indoor air dry bulb (DB)
- •50% relative humidity (rH)
- •95° outdoor air (ODA)

A typical A/C unit is engineered to operate at optimal efficiency and rated capacity under a single set of conditions.





AHRI Design Conditions

67° Wet bulb (Wb)
95° outdoor air (ODA)

When close to design 12° Superheat 10° Subcooling



Table RD-2: Target Superheat (Suction Line Temperature - Evaporator Saturation Temperature) (continued)

Table	KD-2.	lary	el St	ipem	eat (Such	JII LIII	ie ie	inper	aluic										iueu)								ŝn
												Retur	n Air	Wet-	Bulb 1	Гетр	eratu	re (°F)									
														(T	return,	wb)												
	V	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76
	91	-50	27	-		(5)	=	-	155	U=	5	-	-	E	6.1	8.1	10.3	12.2	14.1	15.9	17.8	19.7	21.5	23.4	25.2	27.1	28.9	30.8
	92	i <u>u</u> s	14_21	12	<u>.</u>	-	₩.	E 1	42	34	120	_	974	21	5.4	7.5	9.8	11.7	13.5	15.4	17.3	19.2	21.1	22.9	24.8	26.7	28.5	30.4
	93	-	(-(-	-	-	-	(=3)	:-:	S=:	-	-	((-)	-	1-11	6.8	9.2	11.1	13.0	14.9	16.8	18.7	20.6	22.5	24.4	26.3	28.2	30.1
	94	740	-	E E	12	-	29	121	-	79	Ð	22	-	81	-	62	8.7	10.6	12.5	14 4	16.3	18.2	20.2	22 1	24 0	25.9	27.8	29 7
	95	-	341	-	-	-		FA	-	12	-	-	-	¥1	-	5.6	8.1	10.0	12.0	13.9	15.8	17.8	19.7	21.6	23.6	25.5	27.4	29.4
	96	170	87	15	-	151	- 1	(= 1)	10 0 0	87.	1 55	1.51	85	. 1	(=0)	(-)	7.5	9.5	11.4	13.4	15.3	17.3	19.2	21.2	23.2	25.1	27.1	29.0
	97	-	(64)	12-	_	121	20	20	828	-	22	120	944	=	-	828	7.0	8.9	10.9	12.9	14.9	16.8	18.8	20.8	22.7	24.7	26.7	28.7
Œ	98	-	-		-	-	-	(=);	:	-	<u> </u>	- 1	-	:	1-11	:-:	6.4	8.4	10.4	12.4	14.4	16.4	18.3	20.3	22.3	24.3	26.3	28.3
re (°	99	-	-	8	8	•	20	-	-	-	8	-	-	=	-	-	5.8	7.9	9.9	11.9	13.9	15.9	17.9	19.9	21.9	24.0	26.0	28.0
ratu	100	-	3141	-	i -	54.	-	-	-	-	-	-	7-	= 1	=	-	5.3	7.3	9.3	11.4	13.4	15.4	17.5	19.5	21.5	23.6	25.6	27.7
npe	101	-50	2=	-	-	3.73	-		1.52	1/5	5	1 - 2		-	(=)	(-)	-	6.8	8.8	10.9	12.9	15.0	17.0	19.1	21.1	23.2	25.3	27.3
Ter	102	120	1621	112	-	_	<u></u>	60	-	34	122	128	10121	2 1	-	828	20	6.2	8.3	10.4	12.4	14.5	16.6	18.6	20.7	22.8	24.9	27.0
3nlb	103	-	-	-	-	-	-	(- 1)	:-:	-	-		-	<u>.</u>	-	:-:	_	5.7	7.8	9.9	11.9	14.0	16.1	18.2	20.3	22.4	24.5	26.7
Ory-	104	-	-	B	2	-	29	1-)	-	-		-	-	(1) (2)	-	-	2	5.2	7.2	9.3	11.5	13.6	15.7	17.8	19.9	22.1	24.2	26.3
Air	105	-	341	-	12	-	=	F= N	-	-	-	-	-	¥1	-	4	2	-	6.7	8.8	11.0	13.1	15.2	17.4	19.5	21.7	23.8	26.0
ser	106	-	2.71	15	-		-		100		15	-	87	51	(-)	-	-	3-3	6.2	8.3	10.5	12.6	14.8	17.0	19.1	21.3	23.5	25.7
Condenser Air Dry-Bulb Temperature (°F)	107	120	742	2	_	_	40	-	14	-	<u> </u>	_	934	=	20	-	2	2.	5.7	7.9	10.0	12.2	14.4	16.6	18.7	21.0	23.2	25.4
Cor	108	-	-	-	-	-	-	(=1)	-	-	-	-	-	-	-	:-:	L		5.2	7.4	9.5	11.7	13.9	16.1	18.4	20.6	22.8	25.1
	109	-	-	8	2	-	29	-	-	-	8	-	-	(1) (2)	-	-	2	-	-	6.9	9.1	11.3	13.5	15.7	18.0	20.2	22.5	24.7
	110	4.8	4 <u>0</u> 1		1 1	19/24	42	4211	020	(<u>*</u>	112	1 548	27.27	<u>u</u> 1	120	520	1123	ties 1		64	26						22.1	

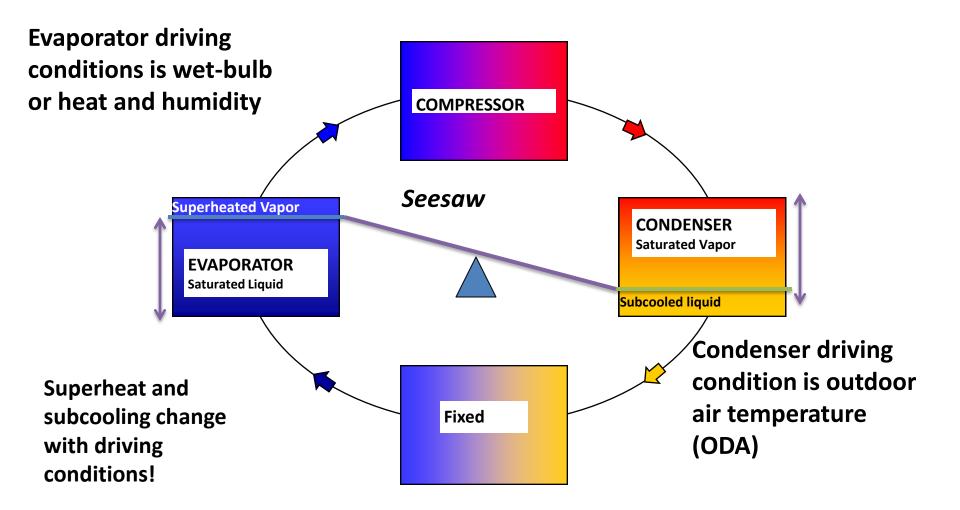


The Fixed Orifice System (Piston)

- Critically charged under all load conditions
- Charged by total superheat method
- Has a target superheat which must be calculated or derived
- Varies in capacity with load conditions
- Simple, but not as efficient at removing heat and humidity under a varying load



The Fixed Orifice System

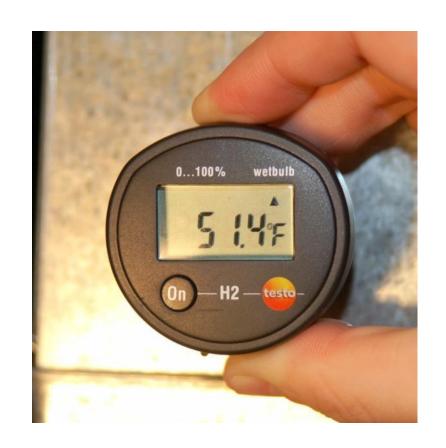




Charging by Total Superheat (Fixed)

Superheat

- Measure outdoor temperature (D/B)
- Measure indoor wet bulb (W/B)
- Charge by total superheat method
- Measure pressure and temperature at condenser inlet





At a constant indoor Wb as outdoor air temp increases, superheat decreases

Table RD-2: Target Superheat (Suction Line Temperature - Evaporator Saturation Temperature)

Tabl	e ND	-2. 1	argei	Supe	inea	l (Su	CHOIT	LITTE	remp	Jerali									/									 î
		\bigcirc	ıtda	oor	۸ir	Dri	ivin	σ E	orce	_		Retur	n Air	Wet-	Bulb	emp	eratu	re (°F)									
		5	itu	JUI	AII	ווט		gr	JIC			2	160	(T	return, v	vb)	· · · · · · · · · · · · · · · · · · ·	00	s		300	ic 16	2 100	Xe: 3	10 10		200	30
		50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76
	55	8.8	10.1	11.5	12.8	14.2	15.6	17.1	18.5	20.0	21.5	23.1	24.6	26.2	27.8	29.4	31.0	32.4	33.8	35.1	36.4	37.7	39.0	40.2	41.5	42.7	43.9	45.0
	56	8.6	9.9	11.2	12.6	14.0	15.4	16.8	18.2	19.7	21.2	22.7	24.2	25.7	27.3	28.9	30.5	31.8	33.2	34.6	35.9	37.2	38.5	39.7	41.0	42.2	43.4	44.6
	57	8.3	9.6	11.0	12.3	13.7	15.1	16.5	17.9	19.4	20.8	22.3	23.8	25.3	26.8	28.3	29.9	31.3	32.6	34.0	35.3	36.7	38.0	39.2	40.5	41.7	43.0	44.2
	58	7.9	9.3	10.6	12.0	13.4	14.8	16.2	17.6	19.0	20.4	21.9	23.3	24.8	26.3	27.8	29.3	30.7	32.1	33.5	34.8	36.1	37.5	38.7	40.0	41.3	42.5	43.7
	59	7.5	8.9	10.2	11.6	13.0	14.4	15.8	17.2	18.6	20.0	21.4	22.9	24.3	25.7	27.2	28.7	30.1	31.5	32.9	34.3	35.6	36.9	38.3	39.5	40.8	42.1	43.3
	60	7.0	8.4	9.8	11.2	12.6	14.0	15.4	16.8	18.2	19.6	21.0	22.4	23.8	25.2	26.6	28.1	29.6	31.0	32.4	33.7	35.1	36.4	37.8	39.1	40.4	41.6	42.9
	61	6.5	7.9	9.3	10.7	12.1	13.5	14.9	16.3	17.7	19.1	20.5	21.9	23.3	24.7	26.1	27.5	29.0	30.4	31.8	33.2	34.6	35.9	37.3	38.6	39.9	41.2	42.4
	62	6.0	7.4	8.8	10.2	11.7	13.1	14.5	15.9	17.3	18.7	20.1	21.4	22.8	24.2	25.5	27.0	28.4	29.9	31.3	32.7	34.1	35.4	36.8	38.1	39.4	40.7	42.0
1	63	5.3	6.8	8.3	9.7	11.1	12.6	14.0	15.4	16.8	18.2	19.6	20.9	22.3	23.6	25.0	26.4	27.8	29.3	30.7	32.2	33.6	34.9	36.3	37.7	39.0	40.3	41.6
▼	64		6.1	7.6	9.1	10.6	12.0	13.5	14.9	16.3	17.7	19.0	20.4	21.7	23.1	24.4	25.8	27.3	28.7	30.2	31.6	33.0	34.4	35.8	37.2	38.5	39.9	41.2
E .	65	-	5.4	7.0	8.5	10.0	11.5	12.9	14.3	15.8	17.1	18.5	19.9	21.2	22.5	23.8	25.2	26.7	28.2	29.7	31.1	32.5	33.9	35.3	36.7	38.1	39.4	40.8
<u>。</u>	66	-		6.3	7.8	9.3	10.8	12.3	13.8	15.2	16.6	18.0	19.3	20.7	22.0	23.2	24.6	26.1	27.6	29.1	30.6	32.0	33.4	34.9	36.3	37.6	39.0	40.4
ure	67	. 3	-	5.5	7.1	8.7	10.2	11.7	13.2	14.6	16.0	17.4	18.8	20.1	21.4	22.7	24.1	25.6	27.1	28.6	30.1	31.5	33.0	34.4	35.8	37.2	38.6	39.9
rati	68	-) -	6.3	8.0	9.5	11.1	12.6	14.0	15.5	16.8	18.2	19.5	20.8	22.1	23.5	25.0	26.5	28.0	29.5	31.0	32.5	33.9	35.3	36.8	38.1	39.5
be	69	₩	(=))	(+)	5.5	7.2	8.8	10.4	11.9	13.4	14.8	16.3	17.6	19.0	20.3	21.5	22.9	24.4	26.0	27.5	29.0	30.5	32.0	33.4	34.9	36.3	37.7	39.1
Air Dry-Bulb Temperature (°F)	70	<u> </u>	60	828	<u>.</u>	6.4	8.1	9.7	11.2	12.7	14.2	15.7	17.0	18.4	19.7	20.9	22.3	23.9	25.4	27.0	28.5	30.0	31.5	33.0	34.4	35.9	37.3	38.7
D T	71	e 🚍	-	100		5.6	7.3	8.9	10.5	12.1	13.6	15.0	16.4	17.8	19.1	20.3	21.7	23.3	24.9	26.4	28.0	29.5	31.0	32.5	34.0	35.4	36.9	38.3
3nl	72	, = 1	1	19 5 0	-		6.4	8.1	9.8	11.4	12.9	14.4	15.8	17.2	18.5	19.7	21.2	22.8	24.3	25.9	27.4	29.0	30.5	32.0	33.5	35.0	36.5	37.9
y-E	73	= 1	(<u>-</u>	843	2	-	5.6	7.3	9.0	10.7	12.2	13.7	15.2	16.6	17.9	19.2	20.6	22.2	23.8	25.4	26.9	28.5	30.0	31.5	33.1	34.6	36.0	37.5
۵	74	2	-	(*)	-	-	-	6.5	8.2	9.9	11.5	13.1	14.5	15.9	17.3	18.6	20.0	21.6	23.2	24.8	26.4	28.0	29.5	31.1	32.6	34.1	35.6	37.1
Ą	75	-	<u>,, , , , , , , , , , , , , , , , , , ,</u>	0-0			S (9=)	5.6	7.4	9.2	10.8	12.4	13.9	15.3	16.7	18.0	19.4		22.7		25.9	27.5		30.6	32.2	33.7	35.2	36.7
e	76	-	(=)(0+0	=			(-	6.6	8.4	10.1	11.7	13.2	14.7	16.1	17.4	18.9	20.5	22.1	23.8	C. C	27.0	28.6	30.1	31.7	33.3	34.8	36.3
Condenser	77	· E	= 0	625	22	-	-	944	5.7	7.5	9.3	11.0	12.5	14.0	15.4	16.8	18.3	20.0	21.6	23.2	24.9	26.5	28.1	29.7	31.3	32.8	34.4	36.0
pu	78	e 51	(=0	672	-		57.	8975	a i	6.7	8.5	10.2	11.8	13.4	14.8	16.2	17.7	19.4	21.1	22.7	24.4	26.0	27.6	29.2	30.8	32.4	34.0	35.6
ပ္ပ	79		-	-	-	-	(F)		-	5.9	7.7	9.5	11.1	12.7	14.2	15.6	17.1	18.8	20.5	22.2	23.8	25.5	27.1	28.8	30.4	32.0	33.6	35.2
	80	21	141	-	2	-27	-	12		120	6.9	8.7	10.4	12.0	13.5	15.0	16.6	18.3	20.0	10 10 10 10	23.3	STERNING TO	26.7	28.3	29.9	31.6	112000	34.8
	81	<u> </u>	-		-	-	-	-	3	-	6.0	7.9	9.7	11.3	12.9	14.3	16.0	Charles and Co.	19.4				26.2	27.9	29.5	31.2	32.8	34.4
	82		(- 2)	:	.	1900	10.5	875	E.	17.1	5.2	7.1	8.9	10.6	12.2	13.7	15.4	17.2	18.9	20.6	22.3	24.0	25.7	27.4	29.1	30.7	32.4	34.0
	83	-	(=3)	(-)	-	3=33		(=)	-	3-3	0.0	6.3	8.2	9.9	11.6	13.1	14.9	16.6	18.4	20.1	21.8	23.5	25.2	26.9	28.6	30.3	32.0	33.7
1	0.4								l				7.4	00	100	40.5	440	40.4	امحدا	100	04.0	^B-9.	~ a	00	CF T	00	10 A	00.0

At a constant ODA temperature as Wb increases superheat increases

Table RD-2: Target Superheat (Suction Line Temperature - Evaporator Saturation Temperature)

rapi	e RD	-2: 1	arget	Supe	ernea	t (Su	ction	Line	rem	perati	ure -	Evap	orato	r Sat	uratic	n re	mper	ature)									
											- 1	Retur	n Air	Wet-I	Bulb 1	Temp	eratu	re (°F) _									
											→			(T	return, v	vb)			E	vap	ora	atoı	r Dr	rivir	ig F	orc	e	
		50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76
	55	8.8	10.1	11.5	12.8	14.2	15.6	17.1	18.5	20.0	21.5	23.1	24.6	26.2	27.8	29.4	31.0	32.4	33.8	35.1	36.4	37.7	39.0	40.2	41.5	42.7	43.9	45.0
	56	8.6	9.9	11.2	12.6	14.0	15.4	16.8	18.2	19.7	21.2	22.7	24.2	25.7	27.3	28.9	30.5	31.8	33.2	34.6	35.9	37.2	38.5	39.7	41.0	42.2	43.4	44.6
	57	8.3	9.6	11.0	12.3	13.7	15.1	16.5	17.9	19.4	20.8	22.3	23.8	25.3	26.8	28.3	29.9	31.3	32.6	34.0	35.3	36.7	38.0	39.2	40.5	41.7	43.0	44.2
	58	7.9	9.3	10.6	12.0	13.4	14.8	16.2						24.8										38.7		41.3	42.5	43.7
	59	7.5	8.9	10.2	11.6	13.0	14.4	15.8	17.2		20.0	the second	and the same of th	24.3			28.7							38.3		40.8	42.1	43.3
	60	7.0	8.4	9.8	11.2	12.6	14.0	15.4	16.8	100000000000000000000000000000000000000			22.4	23.8	1000	26.6	30000000		31.0					12.11.12.11.12.11	39.1	40.4	41.6	42.9
	61	6.5	7.9	9.3	10.7	12.1	13.5	14.9	16.3	17.7	19.1	20.5	21.9	23.3	24.7	26.1	27.5	29.0	30.4	31.8	33.2	34.6	35.9		38.6	39.9	41.2	42.4
	62	6.0	7.4	8.8	10.2	11.7	13.1	14.5	15.9	17.3	18.7	20.1	21.4	22.8	24.2	25.5	27.0	28.4	29.9	31.3	32.7	34.1	35.4	36.8	38.1	39.4	40.7	42.0
	63	5.3	6.8	8.3	9.7	11.1	12.6	14.0	15.4	16.8	18.2	19.6	20.9	22.3	23.6	25.0	26.4	27.8	29.3	30.7	32.2	33.6	34.9	36.3	37.7	39.0	40.3	41.6
	64	-	6.1	7.6	9.1	10.6	12.0	13.5	14.9	16.3	17.7	19.0	20.4	21.7	23.1	24.4	25.8	27.3	28.7	30.2	31.6	33.0	34.4	35.8	37.2	38.5	39.9	41.2
·-	65	-	5.4	7.0	8.5	10.0	11.5	12.9	14.3	15.8	17.1	18.5	19.9	21.2	22.5	23.8	25.2	26.7	28.2	29.7	31.1	32.5	33.9	35.3	36.7	38.1	39.4	40.8
(° F	66	=		6.3	7.8	9.3	10.8	12.3	13.8	15.2	16.6	18.0	19.3	20.7	22.0	23.2	24.6	26.1	27.6	29.1	30.6	32.0	33.4	34.9	36.3	37.6	39.0	40.4
ıre	67	3	-	5.5	7.1	8.7	10.2	11.7	13.2	14.6	16.0	17.4	18.8	20.1	21.4	22.7	24.1	25.6	27.1	28.6	30.1	31.5	33.0	34.4	35.8	37.2	38.6	39.9
ratı	68			0=0	6.3	8.0	9.5	11.1	12.6	14.0	15.5	16.8	18.2	19.5	20.8	22.1	23.5	25.0	26.5	28.0	29.5	31.0	32.5	33.9	35.3	36.8	38.1	39.5
be	69	-	(=);	-	5.5	7.2	8.8	10.4	11.9	13.4	14.8	16.3	17.6	19.0	20.3	21.5	22.9	24.4	26.0	27.5	29.0	30.5	32.0	33.4	34.9	36.3	37.7	39.1
em	70	U 1	600	828	20	6.4	8.1	9.7	11.2	12.7	14.2	15.7	17.0	18.4	19.7	20.9	22.3	23.9	25.4	27.0	28.5	30.0	31.5	33.0	34.4	35.9	37.3	38.7
T c	71		-0	100	50	5.6	7.3	8.9	10.5	12.1	13.6	15.0	16.4	17.8	19.1	20.3	21.7	23.3	24.9	26.4	28.0	29.5	31.0	32.5	34.0	35.4	36.9	38.3
III.	72	= 1	200	20 - 20	-	-	6.4	8.1	9.8	11.4	12.9	14.4	15.8	17.2	18.5	19.7	21.2	22.8	24.3	25.9	27.4	29.0	30.5	32.0	33.5	35.0	36.5	37.9
ry-Bulb Temperature (°F)	73	E 1	(4)	840	2	(4)	5.6	7.3	9.0	10.7	12.2	13.7	15.2	16.6	17.9	19.2	20.6	22.2	23.8	25.4	26.9	28.5	30.0	31.5	33.1	34.6	36.0	37.5
	74	1 28	87.1	1880	5	1924		0.5	0.2	9.9	11.5	13.1	14.5	13.9	17.5	10.0	20.0		25.2	24.0				31.1	32.0	34.1	33.0	
Air	75		-	25	- :			5.6	7.4	9.2	10.8	12.4	13.9	15.3	16.7	18.0	19.4	21.1	22.7	24.3	25.9	27.5	29.1	30.6	32.2	33.7	35.2	36.7
se	/0	-	U= 11	8,00	-	3=0	1	(J.E.)	0.0	0.4	10.1	11.7	13.2	14.7	10.1	17.4	10.9		37	1	5000	27.0			31.7	- State 13.	34.6	
Condense		ē =	-	-	2	-	-	9328	5.7	7.5	9.3	11.0	800000000	14.0	15.4	16.8	18.3	CONTRACTOR OF THE PARTY OF THE	21.6	23.2	24.9	Contraction of the Contraction o	COMMUNICIONS	29.7	31.3	32.8	34.4	SON GOODS
ouc	78	8 👨 1	(5.0	672	57	(T.)	\$ 5 7.2	NET	·	6.7	8.5	10.2		13.4			17.7			22.7			27.6		30.8		VE2014-E11	
ŭ	79	E .	100	25=2	=	-		10 -1	=	5.9	7.7	9.5	11.1	12.7	27.700e3V.000	15.6	0000000000000	no-strategy	20.5	- SYSCHOLD STREET	province according	25.5	No Assessment Services	28.8	20000000000000	STREET, PERSON	33.6	
	80	2		-	-	-	1521	35 <u>4</u> 5	-	-	6.9	8.7	10.4	12.0	13.5	15.0	16.6	TEST SEVEN	20.0	-7.11(20/200)	23.3			28.3	29.9	31.6		
	81	3 3	-	-	8	-	•	-	<u></u>	1	6.0	7.9	9.7	11.3	111-10-10-10-10-10-10-10-10-10-10-10-10-	14.3		102 - C. 12 (2.1)	11.100.00	21.1	22.8				29.5	31.2	32.8	0.0000000000000000000000000000000000000
	82	-	-	0.73	=	:= D	-	8758	-	100	5.2	7.1	8.9	10.6		13.7	Market Stone Sto			20.6		24.0			29.1		32.4	
	83	-	(+1)	(=)	=	-	-	(*)	*	-	-	6.3	8.2	9.9	11.6	13.1	14.9	16.6	18.4	20.1	21.8	23.5	25.2	26.9	28.6	30.3	32.0	33.7
-																												

When is the Charge Correct?

- When the actual superheat and the target superheat agree
- There will be some subcooling
 - How much?
 - Who knows? as little as 3 as much as 30

Remember a fixed orifice system is only evaluated for charge by the total superheat of the system.



The TXV System





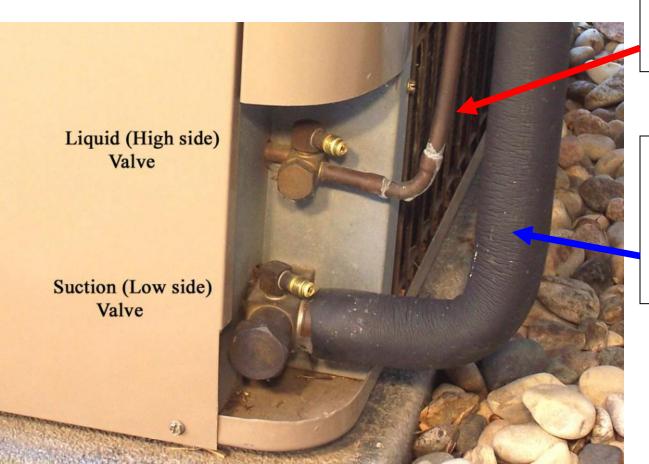
Thermal Expansion Valve

- Critically charged at full load
- Charged verified by condenser subcooling
- Maintains a constant superheat (8-12º typical)
- Maintains capacity under a wide range of load conditions
- Better rH removal under a wide range of loads
- Capable of maintaining a constant suction pressure independent of ODA temp.
- If installed properly, as reliable as a fixed orifice



Probe Positioning

Superheat and subcooling are measured at access ports



TXV

Measure subcooling

Fixed

Measure total superheat



TXV Systems

- 1. Find required subcooling from equipment tag
- 2. Charge directly by subcooling to required level
- 3. Verify P/T and evaporator superheat



Subcooling Notes

The metering device needs to see 4 to 6° of subcooling immediately before its inlet to minimize flash gas.

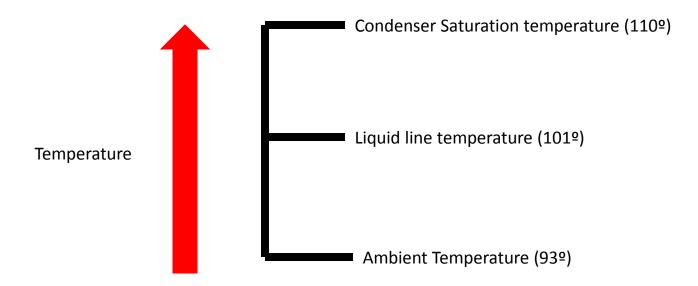
Flash Gas:

- Lowers system efficiency
- Lowers capacity (decrease in mass flow)
- Can damage the metering device
- Temperature drop in the liquid line <u>can</u> indicate problems
- Install a sight glass right before the metering device if desired

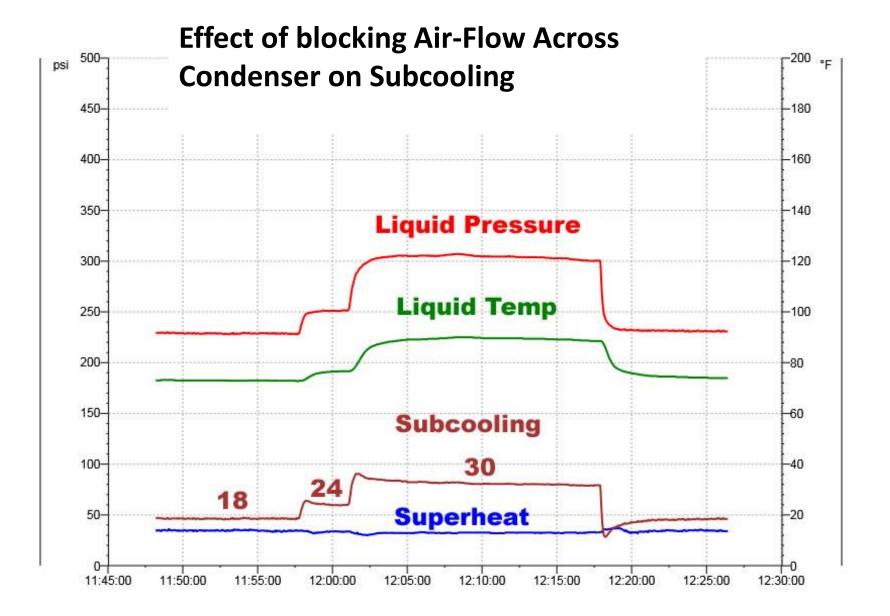


Subcooling and Approach Relationship

Approach = liquid line temp – ambient (8°) Subcooling = condenser saturation temp – liquid line temp (9°) Condensing temp over ambient (split) = (17°)









Real-Time Superheat & Subcooling

Dual temperature inputs

Direct display of superheat and subcooling

Calculated for 33 refrigerants including R22 and 410a

See what is happening not what happened

See minimum (min) maximum (max) and mean (Mean) readings during charging





Verify Both Sides!

- Temperatures
- Pressures
- Coil temperatures
- Superheat
- Subcooling



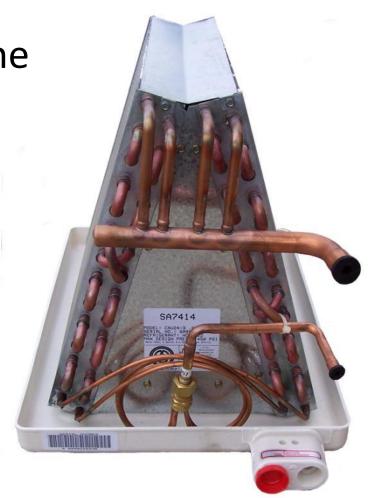
One side can lie about performance!



Verify Temperature Split

Split assures that there that the airflow and the refrigerant charged are proportional.

- Verifies proper operation
- Proper rH removal
- Optimal performance





Evaporator Temperature Drop 20°???

Evaporator temperature drop varies with the R/A humidity

It can be 16-24 degrees with ease!!



Split at ARI Design Conditions

2005 Residential ACM Manual Page RD-9

Table RD-3: Target Temperature Split (Return Dry-Bulb – Supply Dry-Bulb)

				4					A.	<i>x</i> :	F	Returi	n Air \	Wet-E	Bulb (°	F) (T	eturn, wb	₀)										
		50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76
70	0	20.9	20.7	20.6	20.4	20.1	19.9	19.5	19.1	18.7	18.2	17.7	17.2	16.5	15.9	15.2	14.4	13.7	12.8	11.9	11.0	10.0	9.0	7.9	6.8	5.7	4.5	3.2
7	1	21.4	21.3	21.1	20.9	20.7	20.4	20.1	19.7	19.3	18.8	18.3	17.7	17.1	16.4	15.7	15.0	14.2	13.4	12.5	11.5	10.6	9.5	8.5	7.4	6.2	5.0	3.8
7:	2	21.9	21.8	21.7	21.5	21.2	20.9	20.6	20.2	19.8	19.3	18.8	18.2	17.6	17.0	16.3	15.5	14.7	13.9	13.0	12.1	11.1	10.1	9.0	7.9	6.8	5.6	4.3
7:	3	22.5	22.4	22.2	22.0	21.8	21.5	21.2	20.8	20.3	19.9	19.4	18.8	18.2	17.5	16.8	16.1	15.3	14.4	13.6	12.6	11.7	10.6	9.6	8.5	7.3	6.1	4.8
7	4	23.0	22.9	22.8	22.6	22.3	22.0	21.7	21.3	20.9	20.4	19.9	19.3	18.7	18.1	17.4	16.6	15.8	15.0	14.1	13.2	12.2	11.2	10.1	9.0	7.8	6.6	5.4
7	5	23.6	23.5	23.3	23.1	22.9	22.6	22.2	21.9	21.4	21.0	20.4	19.9	19.3	18.6	17.9	17.2	16.4	15.5	14.7	13.7	12.7	11.7	10.7	9.5	8.4	7.2	5.9
7	6	24.1	24.0	23.9	23.7	23.4	23.1	22.8	22.4	22.0	21.5	21.0	20.4	19.8	19.2	18.5	17.7	16.9	16.1	15.2	14.3	13.3	12.3	11.2	10.1	8.9	7.7	6.5
7	7	124	24.6	24.4	24.2	24.0	23.7	23.3	22.9	22.5	22.0	21.5	21.0	20.4	19.7	19.0	18.3	17.5	16.6	15.7	14.8	13.8	12.8	11.7	10.6	9.5	8.3	7.0
78	8	-		-	24.7	24.5	24.2	23.9	23.5	23.1	22.6	22.1	21.5	20.9	20.2	19.5	18.8	18.0	17.2	16.3	15.4	14.4	13.4	12.3	11.2	10.0	8.8	7.6
79	9	_		ī	F	-	24.8	24.4	24.0	23.6	23.1	22.6	22.1	21.4	20.8	20.1	19.3	18.5	17.7	16.8	15.9	14.9	13.9	12.8	11.7	10.6	9.4	8.1
80	0			: 8	æ	÷1	-	25.0	24.6	24.2	23.7	23.2	22.6	22.0	21.3	20.6	19.9	19.1	18.3	17.4	16.4	15.5	14.4	13.4	12.3	11.1	9.9	8.7
8	1		-	-	-	-	-	-	25.1	24.7	24.2	23.7	23.1	22.5	21.9	21.2	20.4	19.6	18.8	17.9	17.0	16.0	15.0	13.9	12.8	11.7	10.4	9.2
82	2	•		14	-	-	-	1,=	-	25.2	24.8	24.2	23.7	23.1	22.4	21.7	21.0	20.2	19.3	18.5	17.5	16.6	15.5	14.5	13.4	12.2	11.0	9.7
8:	3	120	-	Ť	ř	+	-	-	-	75	25.3	24.8	24.2	23.6	23.0	22.3	21.5	20.7	19.9	19.0	18.1	17.1	16.1	15.0	13.9	12.7	11.5	10.3
84	4	-	-	-	-	-	-	-) -	-	25.9	25.3	24.8	24.2	23.5	22.8	22.1	21.3	20.4	19.5	18.6	17.6	16.6	15.6	14.4	13.3	12.1	10.8



Split at Typical Operating Conditions

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Table RD-3: Target Temperature Split (Return Dry-Bulb – Supply Dry-Bulb)

											F	Returi	n Air \	Wet-B	ulb (°	F) (T _r	eturn, wb	₅)	V.00							Mar.		
127		50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76
8	70	20.9	20.7	20.6	20.4	20.1	19.9	19.5	19.1	18.7	18.2	17.7	17.2	16.5	15.9	15.2	14.4	13.7	12.8	11.9	11.0	10.0						
10	71	21.4	21.3	21.1	20.9	20.7	20.4	20.1	19.7	19.3	18.8	18.3	17.7	17.1	16.4	15.7	15.0	14.2	13.4	12.5	11.5	10.6	9.5					
3	72	21.9	21.8	21.7	21.5	21.2	20.9	20.6	20.2	19.8	19.3	18.8	18.2	17.6	17.0	16.3	15.5	14.7	13.9	13.0	12.1	11.1	10.1	9.0				
, db)	73	22.5	22.4	22.2	22.0	21.8	21.5	21.2	20.8	20.3	19.9	19.4	18.8	18.2	17.5	16.8	16.1	15.3	14.4	13.6	12.6	11.7	10.6	9.6	8.5			
(T return, db)	74	23.0	22.9	22.8	22.6	22.3	22.0	21.7	21.3	20.9	20.4	19.9	19.3	18.7	18.1	17.4	16.6	15.8	15.0	14.1	13.2	12.2	11.2	10.1	9.0	7.8		
	75	23.6	23.5	23.3	23.1	22.9	22.6	22.2	21.9	21.4	21.0	20.4	19.9	19.3	18.6	17.9	17.2	16.4	15.5	14.7	13.7	12.7	11.7	10.7	9.5	8.4	7.2	
Return Air Dry-Bulb (°F)	76	24.1	24.0	23.9	23.7	23.4	23.1	22.8	22.4	22.0	21.5	21.0	20.4	19.8	19.2	18.5	17.7	16.9	16.1	15.2	14.3	13.3	12.3	11.2	10.1	8.9	7.7	6.5
Bull	77	1000	24.6	24.4	24.2	24.0	23.7	23.3	22.9	22.5	22.0	21.5	21.0	20.4	19.7	19.0	18.3	17.5	16.6	15.7	14.8	13.8	12.8	11.7	10.6	9.5	8.3	7.0
Ory-	78	-	t#		24.7	24.5	24.2	23.9	23.5	23.1	22.6	22.1	21.5	20.9	20.2	19.5	18.8	18.0	17.2	16.3	15.4	14.4	13.4	12.3	11.2	10.0	8.8	7.6
AIL	79	1572	75			-	24.8	24.4	24.0	23.6	23.1	22.6	22.1	21.4	20.8	20.1	19.3	18.5	17.7	16.8	15.9	14.9	13.9	12.8	11.7	10.6	9.4	8.1
E	80	-	1141	-	- O¥	20	-	25.0	24.6	24.2	23.7	23.2	22.6	22.0	21.3	20.6	19.9	19.1	18.3	17.4	16.4	15.5	14.4	13.4	12.3	11.1	9.9	8.7
Ret	81	1500	867	3	Ē.	-	176		25.1	24.7	24.2	23.7	23.1	22.5	21.9	21.2	20.4	19.6	18.8	17.9	17.0	16.0	15.0	13.9	12.8	11.7	10.4	9.2
9	82	-	t e	-	-	2	-	0.40	-	25.2	24.8	24.2	23.7	23.1	22.4	21.7	21.0	20.2	19.3	18.5	17.5	16.6	15.5	14.5	13.4	12.2	11.0	9.7
	83		F94			=	ATE:	177	13		25.3	24.8	24.2	23.6	23.0	22.3	21.5	20.7	19.9	19.0	18.1	17.1	16.1	15.0	13.9	12.7	11.5	10.3
200	84	343	SE8	P	P	an .		922	22	2	25.9	25.3	24.8	24.2	23.5	22.8	22.1	21.3	20.4	19.5	18.6	17.6	16.6	15.6	14.4	13.3	12.1	10.8



TruTech Recommended Tools

- Testo 5XX series manifold or Digi-Cool AK900
- Testo 605-H2 Psychrometer (for Wet bulb)
- Testo 416 or Fieldpiece STA-2 (for airflow)
- Testo 318-V Video scope for inspections
- Testo 510 for static pressure
- TTT Static pressure test kit
- TTT Troubleshooting guides





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